American Journal of Mathematics and Sciences Vol. 5, No.1, (January-December, 2016) Copyright © Mind Reader Publications ISSN No: 2250-3102 <u>www.journalshub.com</u>

# EFFECT OF POROUS MEDIUM ON MHD UNSTEADY FLOW OF OLDROYD FLUID THROUGH RECTANGULAR CHANNEL

DR. PAVAN SHARMA (Assot. Prof. Dept Of Mathematics) sanjay institute of engg. & mgmt, mathura(u.p.)

AND

PROF. (DR.)C.B.GUPTA EX-HEAD P.G. DEPTT OF MATHEMATICS B.S.A (PG) COLLEGE MATHURA(U.P.)

#### Abstract

The purpose of present study is to analyze the effect of porous medium on MHD unsteady flow of Oldroyd fluid through a rectangular channel in the presence of magnetic field. Here we considered the first and second order Oldroyd fluid and investigate the same problem in this new visco-elastic model. The numerical expressions of the velocity profiles have been given for both first and second order fluids.

Keywords- Porous Medium, Mhd Flow, Oldroyd Fluid Hartmann Number, Porosity Parameter, Fourier Series.

## INTRODUCTION

The study of the physics of flow through porous medium has become the basis of many scientific and engineering applications. This type of flow is of great importance in the petroleum engineering concerned with the movement of oil, gas and water through the reservoir of an oil or gas field to the hydrologist in the study of the migration of underground water and to the chemical engineer in the filtration process.

In the classical theory of viscous flow tremendous development have been observed as evidenced by the informative monographs of Batchelor [1] and various other authors Maity et. al [9], Kumar [4], Kundu and Sengupta [5], Sharma [11], Kundu and Sengupta [6], Rahman and Alam Sarkar [10], Varshney and Singh [12], Kumar and Singh [3], Mahdy [7], Mahdy et al [8], Hayat et al [2] and Varshney and Singh [13].

In recent years the development of new areas of fluid mechanics are very remarkable. For this one may refer to the review of literature in the connection with non-Newtonian fluids, polymetric liquids and visco-elastic liquids of different types with porous medium.

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Moreover some interesting problems in this area have been investigated by Kumar [3] and his research collaborators.

In the present study we have considered the problem of Kumar [3] with porous medium.

## Basic theory and equations of motion for first order Oldroyd fluid

For slow motion, the rheological equations for Oldroyd visco-elastic fluid are:

$$\begin{aligned} \tau_{ij} &= -p' \delta_{ij} + \tau'_{ij} \\ \left( 1 + \lambda'_{1} \frac{\partial}{\partial t'} \right) \tau'_{ij} &= 2\mu \left( 1 + \mu'_{1} \frac{\partial}{\partial t'} \right) e_{ij} \\ e_{ij} &= \frac{1}{2} \left( v_{i,j} + v_{j,i} \right) \end{aligned}$$

and

where  $\tau_{ij}$  is the stress tensor,  $\tau'_{ij}$  is the deviatoric stress tensor,  $e_{ij}$  is the rate of strain tensor, p' is the pressure,  $\lambda'_{i}$  is the stress relaxation time parameter,  $\mu'_{i}$  is the strain rate retardation time parameter,  $\delta_{ij}$  is the metric tensor in Cartesian co-ordinates,  $\mu$  is the coefficient of viscosity and  $v_{i,j}$  is the velocity components.

Let us consider the walls of the rectangular channel to the planes  $x' = \pm a$  and  $y' = \pm b$ , where z'-axis is taken towards the direction of motion 0, 0, w' (x', y', t') are respectively the velocity components along x', y', z' direction where w' (x', y', t') is the axial velocity of the fluid. A transient pressure gradient  $-Pe^{-\omega't'}$  varying with time is applied to the fluid.

Following the stress-strain relation the equation for unsteady motion is given by

Introducing the non dimensional quantities

$$w = \frac{w'a}{\upsilon}, \qquad p = \frac{p'a^2}{\rho\upsilon^2}, \qquad t = \frac{t'\upsilon}{a^2}$$
$$\omega = \frac{\omega'a^2}{\upsilon}, \qquad (x, y, z) = \frac{1}{a}(x', y', z')$$
$$\lambda_1 = \lambda_1' \frac{\upsilon}{a^2}, \qquad \mu_1 = \mu_1' \frac{\upsilon}{a^2}$$

The equation (1) becomes

$$\left(1+\lambda_{1}\frac{\partial}{\partial t}\right)\frac{\partial w}{\partial t} = \left(1+\lambda_{1}\frac{\partial}{\partial t}\right)\frac{\partial p}{\partial z} + \left(1+\mu_{1}\frac{\partial}{\partial t}\right)\nabla^{2}w - \left(M^{2}+\frac{1}{K}\right)\left(1+\lambda_{1}\frac{\partial}{\partial t}\right)w$$
......(2)

where  $M = aB_0 \sqrt{\frac{\sigma}{\mu}}$  (Hartmann number) and  $K = \frac{1}{a^2}K'$  (Porosity parameter).

The boundary conditions are

w = 0, when x = ±1, 
$$-\frac{b}{a} \le y \le \frac{b}{a}$$
 .....(3)

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w = 0, when 
$$y = \pm \frac{b}{a}$$
,  $-1 \le x \le 1$  .....(4)

From the nature of boundary conditions, we have chosen the solution of (2) as  $w = W(x) \cos my e^{-\omega t}$ .....(5)

Condition (4) will be satisfied if  $\cos m \frac{b}{a} = 0$ 

or

$$m = (2n+1)\frac{\pi a}{2b}$$
,  $n = 0, 1, 2, 3...$  .....(6)

Now the boundary conditions (3) become

W = 0 when  $x = \pm 1$ 

.....(7) We construct the solution as the sum of all possible solutions for each value of n

By putting  $\frac{\partial p}{\partial z} = -Pe^{-\omega t} (\omega > 0)$  in (2) and using (7) we get

$$\sum_{n=0}^{\infty} \left\{ \frac{d^2}{dx^2} W(x) - m^2 W(x) \right\} \cos my + \sum_{n=0}^{\infty} \left\{ \frac{\left(1 - \lambda_1 \omega\right) \left(\omega - M^2 - \frac{1}{K}\right)}{\left(1 - \mu_1 \omega\right)} \right\} W(x) \cos my + \frac{\left(1 - \lambda_1 \omega\right)}{\left(1 - \mu_1 \omega\right)} P = 0 \dots (9)$$

Equating the coefficient of cos my equal to zero, we get

$$\frac{d^{2}}{dx^{2}}W - \frac{K_{1}^{2}}{a^{2}} + A_{n} = 0 \qquad .....(10)$$
$$K_{1}^{2} = \left\{ m^{2} - \frac{(1 - \lambda_{1}\omega)(\omega - M^{2} - \frac{1}{K})}{(1 - \mu_{1}\omega)} \right\} a^{2}$$

where

and

Solving equation (9) and using boundary condition (7) we get

$$W(x) = \frac{(-1)^{n+1} 4P(1-\lambda_1 \omega)}{(2n+1)\pi(1-\mu_1 \omega)K_1^2} \begin{cases} 1 - \frac{\cosh \frac{K_1}{a}x}{\cosh \frac{K_1}{a}} \end{cases}$$

Thus the velocity of the fluid is given by

$$w(x, y, t) = \sum_{n=0}^{\infty} \left[ \frac{(-1)^{n+1} 4P(1-\lambda_{1}\omega)}{(2n+1)\pi(1-\mu_{1}\omega)K_{1}^{2}} \left\{ 1 - \frac{\cosh\frac{K_{1}}{a}x}{\cosh\frac{K_{1}}{a}} \right\} \right] e^{-\omega t} \cos(2n+1)\frac{\pi ay}{2b} \dots (12)$$

Thus equation (12) represents the velocity of first order Oldroyd visco-elastic fluid. Basic theory and equation or motion for second order Oldroyd fluid

Or slow motion, the rheological equations for second order Oldroyd visco-elastic fluid are.

$$\tau_{ij} = -p'\delta_{ij} + \tau'_{ij}$$

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$$\begin{split} & \left(1 + \lambda_{1}^{'} \frac{\partial}{\partial t^{'}} + \lambda_{2}^{'} \frac{\partial^{2}}{\partial t^{'2}}\right) \tau_{ij}^{'} = 2\mu \bigg(1 + \mu_{1}^{'} \frac{\partial}{\partial t^{'}} + \mu_{2}^{'} \frac{\partial^{2}}{\partial t^{'2}}\bigg) e_{ij} \\ & \text{and} \qquad e_{ij} = \frac{1}{2} \Big(v_{i,j} + v_{j,i}\Big) \end{split}$$

where  $\tau_{ij}$  is the stress tensor,  $\tau'_{ij}$  is the deviatoric stress tensor,  $e_{ij}$  is the rate of strain tensor, p' is the pressure,  $\lambda'_1$  is the stress relaxation time parameter,  $\mu'_1$  is the strain rate retardation time parameter,  $\lambda'_2$  is the additional material constant,  $\mu'_2$  is the additional material constant,  $\delta_{ij}$  is the metric tensor in Cartesian co-ordinates,  $\mu$  is the coefficient of viscosity and  $v_i$  is the velocity components.

Let us consider the walls of the rectangular channel to be the planes  $x' = \pm a$  and  $y' = \pm b$ , where z'-axis is taken towards the direction of motion 0, 0, w' (x', y', t') are respectively the velocity components along x', y', z' direction where w' (x', y', t') is the axial velocity of the fluid. A transient pressure gradient  $-Pe^{-\omega't'}$  varying with time is applied to the fluid.

Following the stress-strain relation the equation for unsteady motion is given by

$$\begin{pmatrix} 1 + \lambda_1' \frac{\partial}{\partial t'} + \lambda_2' \frac{\partial^2}{\partial t'^2} \end{pmatrix} \frac{\partial w'}{\partial t'} = -\frac{1}{\rho} \left( 1 + \lambda_1' \frac{\partial}{\partial t'} + \lambda_2' \frac{\partial^2}{\partial t'^2} \right) \frac{\partial p'}{\partial z'}$$
  
+  $\upsilon \left( 1 + \mu_1' \frac{\partial}{\partial t'} + \mu_2' \frac{\partial^2}{\partial t'^2} \right) \nabla^2 w' - \left( \frac{\upsilon}{K'} + \frac{\sigma B_0^{2'}}{\rho} \right) \left( 1 + \lambda_1' \frac{\partial}{\partial t'} + \lambda_2' \frac{\partial^2}{\partial t'^2} \right) w' \dots (13)$ 

Introducing the non dimensional quantities

$$w = \frac{w'a}{\upsilon}, \qquad \omega = \frac{\omega'a^2}{\upsilon} \qquad p = \frac{p'a^2}{\rho\upsilon^2}, \qquad (x, y, z) = \frac{1}{a}(x', y', z')$$
$$t = \frac{t'\upsilon}{a^2}, \qquad \lambda_1 = \lambda_1' \frac{\upsilon}{a^2}, \qquad \mu_1 = \mu_1' \frac{\upsilon}{a^2} \qquad \mu_2 = \mu'\frac{\upsilon^2}{a^4}, \qquad \lambda_2 = \lambda_2' \frac{\upsilon^2}{a^4}$$

in equation (13), we get

where  $M = aB_0 \sqrt{\frac{\sigma}{\mu}}$  (Hartmann number) and  $K = \frac{1}{a^2}K'$  (Porosity parameter).

#### Solution of the problem

 $\alpha$ 

Let the possible solution (14) as

$$w = W(x) \cos my e^{-\omega t}$$

Here we used the same boundary conditions of fluid given by (7) after using (4) and (6). We construct the solution as the sum of all possible solutions for each value of n.

$$w = \sum_{n=0}^{\infty} W(x) \cos my \ e^{-\omega t}$$
 .....(15)

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and 
$$\frac{\partial p}{\partial z} = -Pe^{-\omega t}, (\omega > 0)$$

Using (15) and putting the value of  $\frac{\partial p}{\partial z}$  in (14), we get

$$\sum_{n=0}^{\infty} \left[ \frac{d^2}{dx^2} W(x) - m^2 W(x) \right] \cos my + \frac{\left(1 - \lambda_1 \omega + \lambda_2 \omega^2\right) \left(\omega - M^2 - \frac{1}{K}\right)}{\left(1 - \mu_1 \omega + \mu_2 \omega^2\right)}$$
$$\times \sum_{n=0}^{\infty} W(x) \cos my + \frac{\left(1 - \lambda_1 \omega + \lambda_2 \omega^2\right)}{\left(1 - \mu_1 \omega + \mu_2 \omega^2\right)} P = 0 \qquad \dots \dots (16)$$

If we express  $\frac{(1-\lambda_1\omega+\lambda_2\omega^2)}{(1-\mu_1\omega+\mu_2\omega^2)}P$  as a Fourier series in the interval of  $-\frac{b}{a} \le y \le \frac{b}{a}$ 

and equate the coefficient of cos my to zero, we get

where

$$K_{1}^{2} = \left\{ m^{2} - \frac{\left(1 - \lambda_{1}\omega + \lambda_{2}\omega^{2}\right)\left(\omega - M^{2} - \frac{1}{K}\right)}{\left(1 - \mu_{1}\omega + \mu_{2}\omega^{2}\right)} \right\} a^{2} \qquad \dots \dots (18)$$

Now we obtain the solution by using the boundary condition (7) as follows

$$W(x) = \frac{(-1)^{n+1}}{(2n+1)} \frac{4P}{\pi} \frac{(1-\lambda_1\omega + \lambda_2\omega^2)}{(1-\mu_1\omega + \mu_2\omega^2)K_1^2} \begin{cases} 1\frac{\cos\frac{K_1}{a}x}{\cosh\frac{K_1}{a}} \\ 1\frac{\cos\frac{K_1}{a}x}{\cosh\frac{K_1}{a}} \end{cases}$$

So the velocity of the fluid is given by

$$W(x, y, t) = \frac{(-1)^{n+1}}{(2n+1)} \frac{4P(1-\lambda_1\omega+\lambda_2\omega^2)}{\pi(1-\mu_1\omega+\mu_2\omega^2)K_1^2} \left\{ 1 - \frac{\cos\frac{K_1}{a}x}{\cosh\frac{K_1}{a}} \right\} \times e^{-\omega t} \cos(2n+1)\frac{\pi a y}{2b} \dots (19)$$

Thus the velocity of second order Oldroyd visco-elastic fluid is given by equation (19).

#### DEDUCTION

Case I : If we put  $\mu_1 = 0$  in equation (12) we shall obtain the Maxwell fluid which is given below

$$w(x, y, t) = \sum_{n=0}^{\infty} \left[ \frac{(-1)^{n+1}}{(2n+1)} \frac{4P(1-\lambda_1\omega)}{\pi K_1^2} \left\{ 1 - \frac{\cosh\frac{K_1}{a}x}{\cosh\frac{K_1}{a}} \right\} \right] e^{-\omega t} \cos(2n+1) \frac{\pi ay}{2b}$$
$$K_1^2 = \left[ m^2 - (1-\lambda_1\omega) \left( \omega - M^2 - \frac{1}{K} \right) \right] a^2$$

where

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**Case II** : Putting  $\mu_1 = 0$  and  $\lambda_1 = 0$  in equation (12) we shall obtain the purely viscous fluid which is given below

$$w(x, y, t) = \sum_{n=0}^{\infty} \left[ \frac{(-1)^{n+1}}{(2n+1)} \frac{4P}{\pi K_1^2} \left\{ 1 - \frac{\cosh \frac{K_1}{a} x}{\cosh \frac{K_1}{a}} \right\} \right] e^{-\omega t} (2n+1) \frac{\pi a y}{2b}$$
$$K_1^2 = \left\{ m^2 - \left( \omega - M^2 - \frac{1}{K} \right) \right\} a^2$$

where

**Case III :** Putting K = 0 in equation (12) we shall obtain the same result of Kumar and Singh [3].

## DISCUSSION

The expressions for velocities (in the presence of porous medium) of first order Oldroyd visco-elastic fluid by (12) and for second order visco-elastic fluid is given by equations (19) respectively.

#### Acknowledgement:

The authors are very thankful to the Dr. Ashok kumar agrawal, Principal, B.S.A.(P.G.) College,Mathura and Dr. K. K. Kanodia, the Head P.G. Department of Mathematics B.S.A.(P.G.) College,Mathura for providing necessary facilities and Valuable suggetions also thankful to Lokendra Parashar,Office Assitant Sanjay Institute of Engineering & Management, Mathura for computational help.

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